

$$(i) \quad T_1 = T_0 - \frac{V_1^2}{2c_p} = 402.1 \text{ K} \quad (\text{adiabatic})$$

$$a_1 = \sqrt{\gamma R T_1} = 401.95 \text{ m/s}$$

NOT T_0 ! $\Rightarrow M_1 = \frac{V_1}{a_1} = 1.500$

Alternatively from tables, using $V_1 / \sqrt{c_p T_0} = 0.7878$

$$(ii) \quad \left. \begin{aligned} T_2 &= T_1 + 69 \text{ K} = 471.1 \text{ K} \\ \text{Adiabatic} \Rightarrow T_{02} &= 583 \text{ K} \end{aligned} \right\} \begin{aligned} T_2 / T_{02} &= 0.80806 \\ M_2 &= 1.090 \quad (\text{Tables, or direct calc.}) \end{aligned}$$

Distance to choking at 1: $\left(\frac{4c_f L_{\max}}{D} \right)_1 = 0.1361$

———— " ————— 2: $\left(\frac{4c_f L_{\max}}{D} \right)_2 = 0.0082$

and $(L_{\max})_1 - (L_{\max})_2 = 1.2 \text{ m}$, $D = 0.08 \text{ m}$
 $\Rightarrow c_f = 2.13(17) \times 10^{-3}$

(iii) $\dot{m}$, T_0 , A all constant

$$\frac{\dot{m} \sqrt{c_p T_0}}{A p_{01}} = 1.0891 \quad \frac{\dot{m} \sqrt{c_p T_0}}{A p_2} = 2.6842 \Rightarrow p_2 = 2.0287 \text{ bar}$$

$\uparrow = p_0$ (nozzle frictionless)

a) (iii) cont'd ...

Shock table : $P_3/P_2 = 1.2195 \Rightarrow P_3 = \underline{\underline{2.47 \text{ bar}}}$

N.B. P_3 same as ambient pressure since flow subsonic.

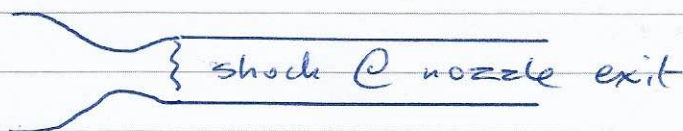
b) (i) To match higher pressure at exit...

either $\rightarrow$ - must reduce friction force $\propto \frac{1}{2}\rho V^2$ (1)

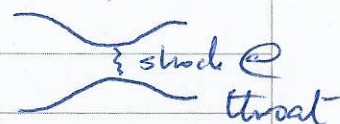
OK $\rightarrow$ - must increase pressure rise across shock (2)

$\Rightarrow$ shock moves upstream - to give more subsonic, low $\frac{1}{2}\rho V^2$, flow (1)
 - to act on flow with higher Mach no. (2)

until we reach



Further rises in back pressure send shock into nozzle,
 as per standard picture, until ...



after which the nozzle unchokes, and mass flow starts to drop.

(ii) 1% in reduction $\Rightarrow \frac{\dot{m} \sqrt{c_p T_{01}}}{A p_{01}} = 0.99 \times 1.0891 = 1.0782$

So now $M_1 = 0.600$ (tables); $[4c_f L_{\max}/D]_1 = 0.4908$

! Note subsonic sol'n $\uparrow$

Use known c_f , D , $\Delta L_{\max}$ for $[4c_f L_{\max}/D]_2 = 0.3629$

Tables: $M_2 = 1.637$ $\frac{\dot{m} \sqrt{c_p T_0}}{A P_2} = 1.4659 \Rightarrow P_2 = 0.7355 p_{01} = \underline{\underline{3.68 \text{ bar}}}$

a) (i) Differentiate gas law: $dp = \rho R dT + RT d\rho$ (A)

Continuity: $\rho V = \text{const} \Rightarrow \frac{d\rho}{\rho} + \frac{dV}{V} = 0$

Subs. for $d\rho$ in (A): $dp = \rho R dT - \rho RT \frac{dV}{V}$

and $RT = \frac{a^2}{\gamma}$: $dp = \rho \left[R dT - \frac{a^2}{\gamma} \frac{dV}{V} \right]$
 $\underline{\underline{=}}$

(ii) Frictionless duct $\Rightarrow p + \rho V^2 = \text{const}$

N.B. NOT
isentropic. Why?

Differentiate, noting that $\rho V = \text{const}$:

$$dp + \rho V dV = 0$$

Eliminate dp : $\left[\frac{a^2}{\gamma} \frac{1}{V} - V \right] dV = R dT$

At max T , $dT = 0 \Rightarrow V^2 = \frac{a^2}{\gamma}$, $M = \frac{1}{\sqrt{\gamma}}$
 $\underline{\underline{=}}$

b) (i) Stagnation density $\rho_0 = \frac{p_0}{RT_0} = 2.5489 \text{ kg/m}^3$

$\rho_0 = \rho \left[1 + \frac{\gamma-1}{2} M^2 \right]^{\frac{1}{\gamma-1}} \Rightarrow M = 0.400$ (or from
 $\underline{\underline{=}}$ tabulated ρ/ρ_0)

Tables: $\frac{V}{\sqrt{\gamma T_0}} = 0.2490 \Rightarrow V = 130.5 \text{ m/s}$
 $\underline{\underline{=}}$

b)(ii) Use $F (= (\rho + \rho V^2)A) = \text{const}$

N.B. NOT p_0
= const. Why?

	Inlet	Choked	
M	0.4	1	
$F / \sqrt{\dot{m} c_p \bar{T}_0}$	1.3608	0.9897	} $\Rightarrow \frac{\bar{T}_{0c}}{\bar{T}_{0i}} = 1.8905$
	$\bar{T}_0 = \bar{T}_{0i}$	$\bar{T}_0 = \bar{T}_{0c}$	
	$= 273.4K$		

$$\bar{T}_{0c} = 516.9K$$

Also need $\dot{m} = \rho AV = 1.537 \text{ kg/s}$ (from (i))

$$\dot{Q} = \dot{m} c_p \Delta \bar{T}_0 = \underline{\underline{376 \text{ kW}}} \quad \text{+ve, hence heat added to flow}$$

(iii) At $M = \gamma^{-1/2} = 0.845$, $F / \sqrt{\dot{m} c_p \bar{T}_{0m}} = 1$
 $\uparrow \bar{T}_0 \in \text{max } T$

Following same route as (ii): $\bar{T}_{0m} = 506.3K$

$$\dot{Q} = \dot{m} c_p (\bar{T}_{0m} - \bar{T}_{0c}) = \underline{\underline{-16 \text{ kW}}}$$

-ve, hence heat removed from flow.

(iv) Cooling can alternatively take the flow away from the choked condition to supersonic:

$$F / \sqrt{\dot{m} c_p \bar{T}_0} = 1 \quad \text{also @ } M = 1.196$$

with $\bar{T}_0 = \bar{T}_{0m}$ again
and $\dot{m} = 1.537 \text{ kg/s}$ still

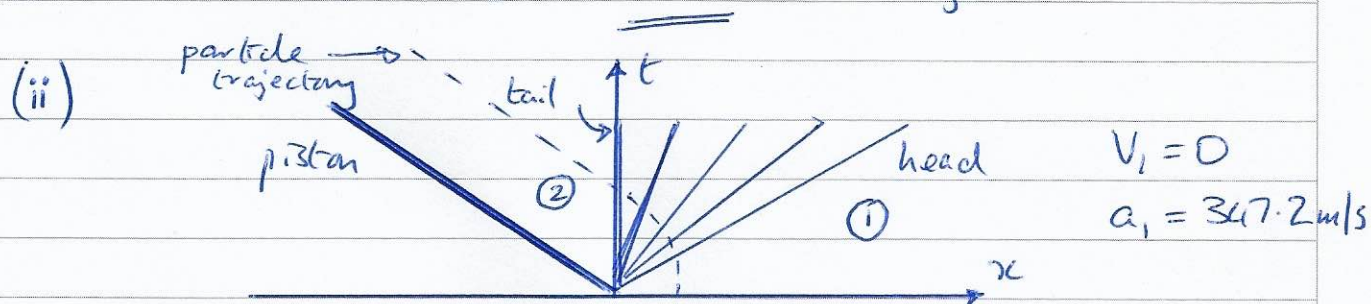
N.B. Two more quantities needed to define gas state.

a) (i) Right-running waves, ^{velocity(!)} ~~speed~~ in laboratory frame is $V + a$, with: V flow velocity
 a local sound speed

Head moves into stationary fluid with $V = 0$

$$a = \sqrt{\gamma R T} = 347.2 \text{ m/s}$$

So head travels @ 347.2 m/s to right

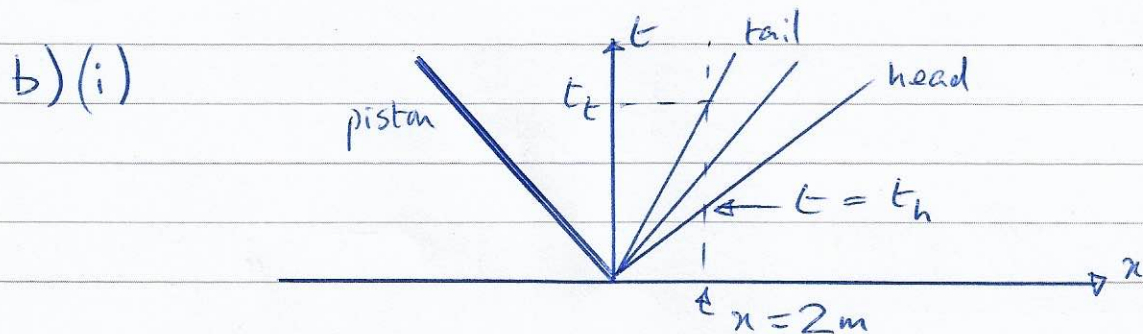


(iii) Across r-r waves: $V_2 - \frac{2}{\gamma-1} a_2 = V_1 - \frac{2}{\gamma-1} a_1$

Tail speed: $V_2 + a_2 = 0$

Solve to obtain $a_2 = 289.3 \text{ m/s}$, $V_2 = -289.3 \text{ m/s}$

Piston speed is same as flow speed in (2): 289 m/s



First variation detected by mike at $t = t_h = 2/347.2 = 5.76 \text{ ms}$

Duration of 30 ms $\Rightarrow t_t = 35.76 \text{ ms}$

b)(i) cont'd

Hence tail speed = $2 / 0.03576 = 55.9 \text{ m/s}$

Across r-r waves $V_2 - \frac{2}{\gamma-1} a_2 = V_1 - \frac{2}{\gamma-1} a_1 = -\frac{2}{\gamma-1} a_1$

Tail velocity $V_2 + a_2 = 55.9$

Solve to obtain $a_2 = 298.65 \text{ m/s}$, $V_2 = -242.75 \text{ m/s}$

Piston speed 243 m/s

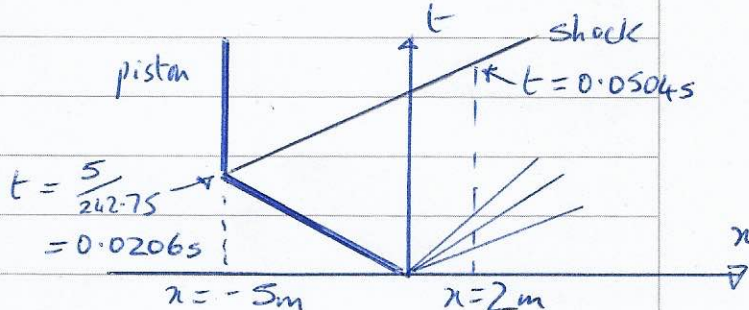
Expansion wave system is Bernoulli,
so... $\frac{P_2}{P_1} = \left(\frac{T_2}{T_1}\right)^{\gamma/(\gamma-1)} = \left(\frac{a_2}{a_1}\right)^{2\gamma/(\gamma-1)}$

BUT can't say $p_0 = \text{const!}$
Why?

giving $P_2 = \underline{0.348 (40) \text{ bar}}$

(ii) When the piston stops, a shock-wave is generated.
The change in pressure detected by the mike marks the shock arrival.

New wave diagram:



Shock travels 7m in 0.0298s $\Rightarrow$ speed is 234.90 m/s
 $\rightarrow 234.9 \text{ m/s}$

Lab frame: $V = 0$ } $\leftarrow 242.75 \text{ m/s}$
(3) } (2) 0.3484 bar

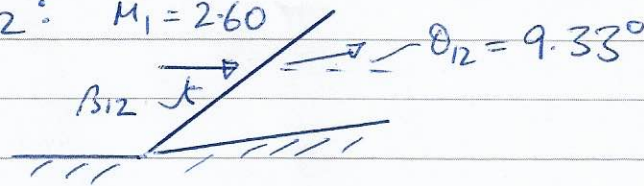
In shock frame, $M = 1.60$

Shock frame: 234.9 m/s } 477.65 m/s
 $\leftarrow$ } $a_2 = 298.65 \text{ m/s}$

Tables: $P_3/P_2 = 2.820$

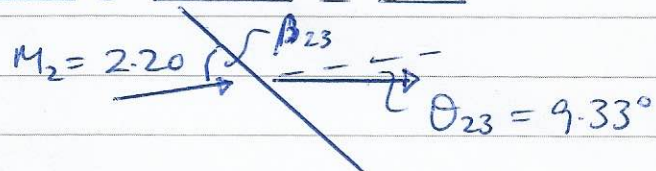
$P_3 = 0.982 \text{ bar}$

a) (i) Across S_{12} : $M_1 = 2.60$

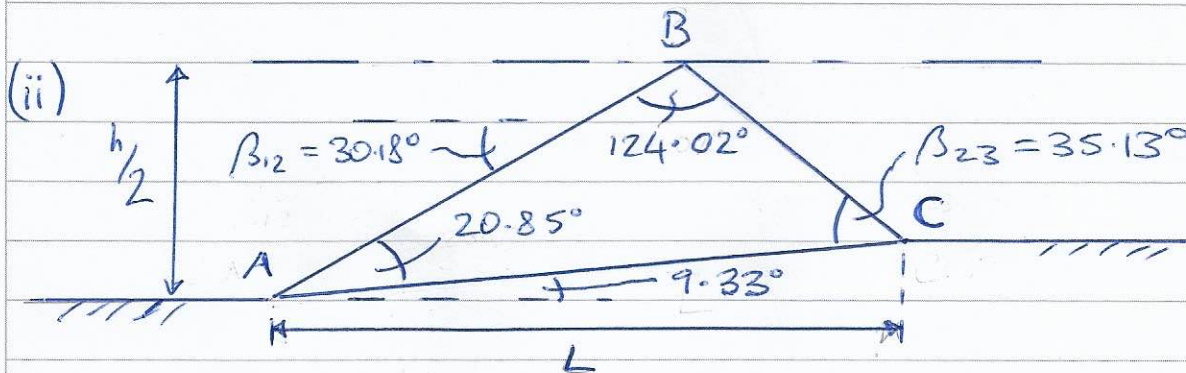


Tables: $M_2 = 2.20$ ($\beta_{12} = 30.18^\circ$)

Across S_{23} :



Tables: $M_3 = 1.85$ ($\beta_{23} = 35.13^\circ$)



$$AB = \frac{h/2}{\sin 30.18^\circ} = 0.995h$$

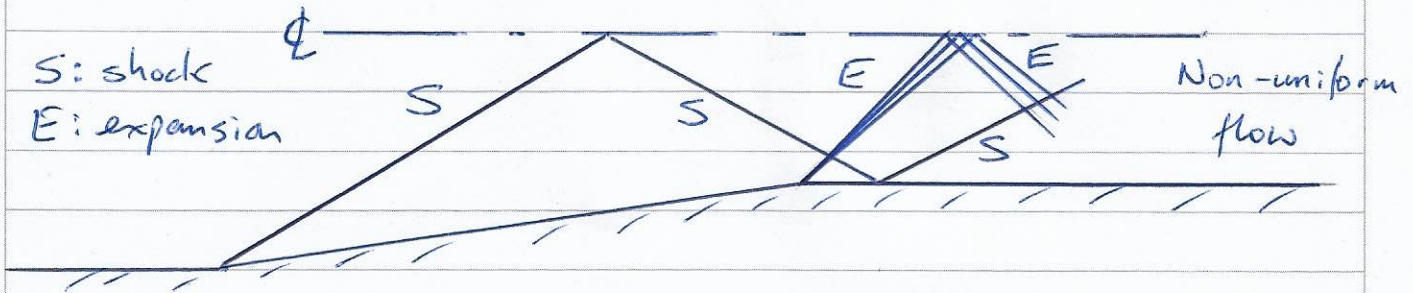
Sine rule: $AC = AB \frac{\sin 124.02^\circ}{\sin 35.13^\circ} = 1.433h$

$$L = AC \cos 9.33^\circ = 1.41h$$

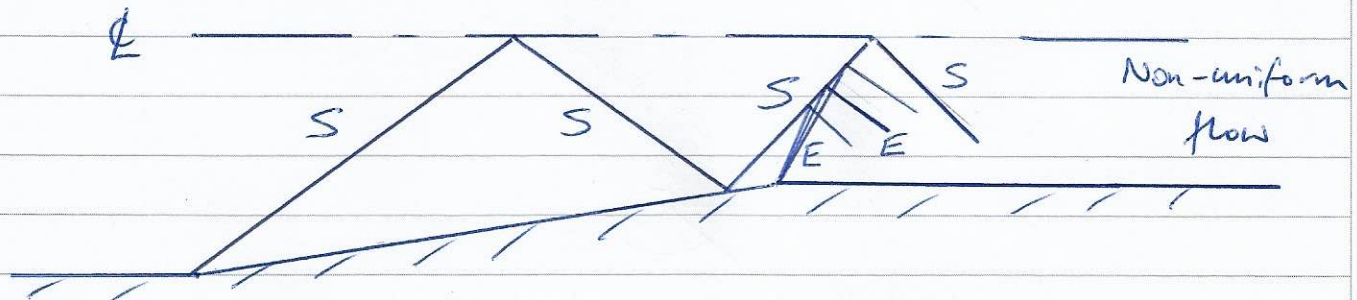
Measurement from a reasonably careful scale drawing also acceptable.

(iii) Tables: $P_{2/P_1} = 1.8272$

b)(i) Increased $M \rightarrow$ decreased β_{12}

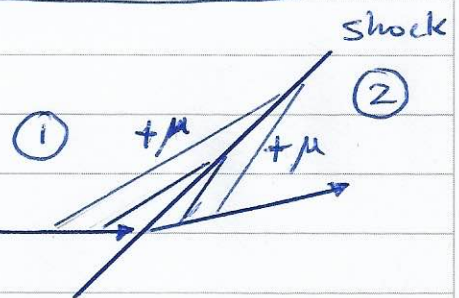


(ii) Decreased $M \rightarrow$ increased β_{12}



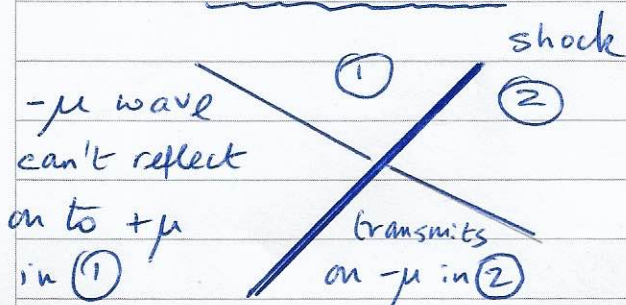
A NOTE ON INTERACTIONS BETWEEN SHOCKS AND EXPANSIONS

Oblique shock angles are such that similarly inclined characteristics intersect the shock on both sides $\rightarrow$

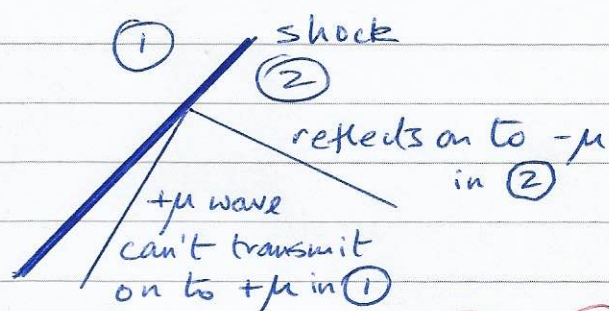


This observation determines whether a wave is transmitted or reflected:

Transmission



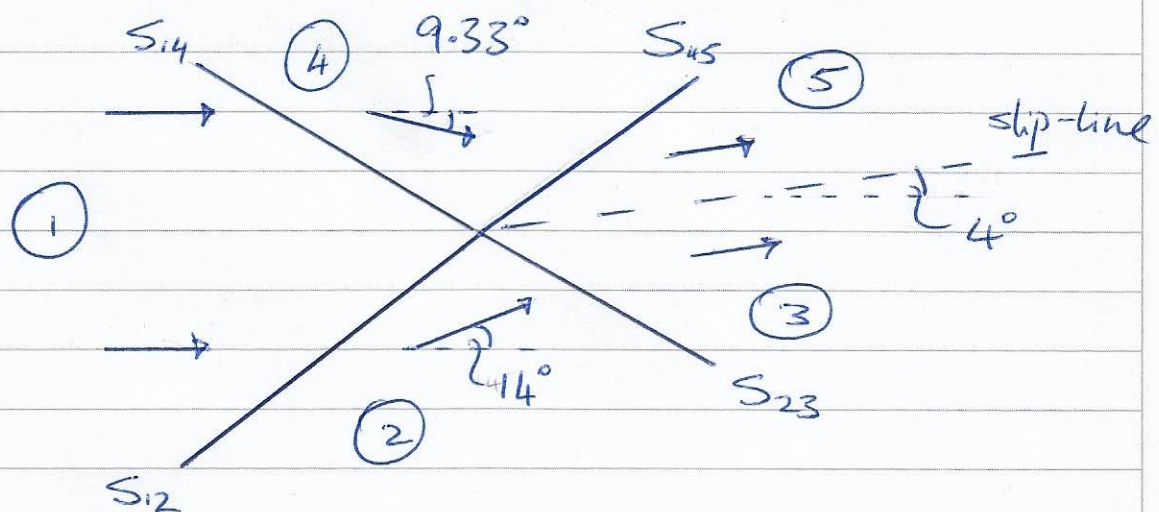
Reflection



c) The flow is now asymmetric, with a slip-line emanating from the shock intersection.

Across a slip-line ... velocities parallel, speeds differ
pressures equal

Assume the researcher is correct:



$$S_{12}: M_2 = 2.00 \quad \cancel{P_2/P_1} \quad P_2/P_1 = 2.3955$$

$$S_{23}: \theta_{23} = 10^\circ \quad P_3/P_2 = 1.7066 \quad \boxed{P_3 = 4.088 p_1}$$

$$S_{14} \text{ unchanged: } M_4 = 2.20 \quad P_4/p_1 = 1.8272$$

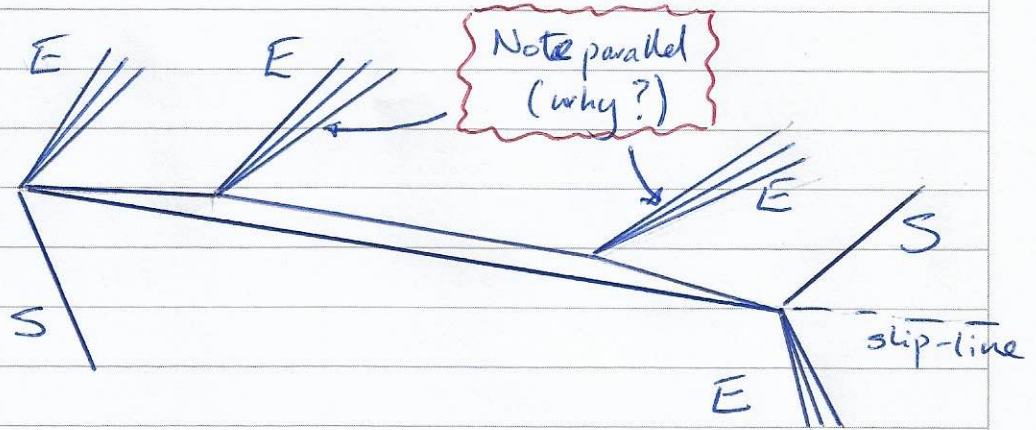
$$S_{45}: \theta_{45} = 13.33^\circ \quad P_5/p_4 = 2.1037 \quad \boxed{P_5 = 3.844 p_1}$$

p_3 is too high and p_5 too low, so in reality
 S_{23} is weaker than assumed, and S_{45} stronger

$\Rightarrow$ less flow turning through S_{23} and more through S_{45}
 $\Rightarrow$ researcher's estimate is too low, angle $> 4^\circ$.

a)

S: shock
E: expansion

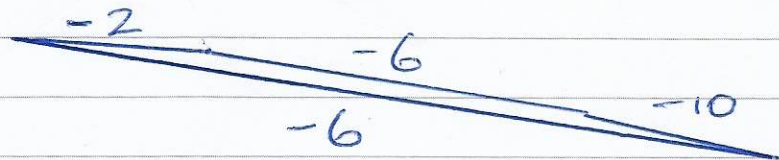


b) Linearised method of characteristics gives

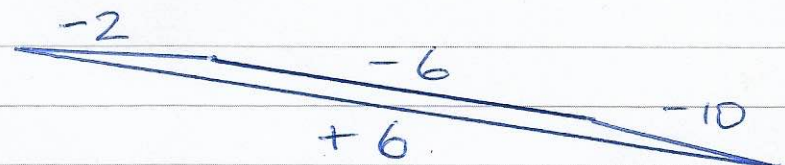
$$\frac{p - p_{\infty}}{\frac{1}{2} \rho_{\infty} U_{\infty}^2} = \pm \frac{2\theta}{\sqrt{M_{\infty}^2 - 1}}$$

Notes: + across μ (upper surface)
- across $-\mu$ (lower surface)
 θ in radians

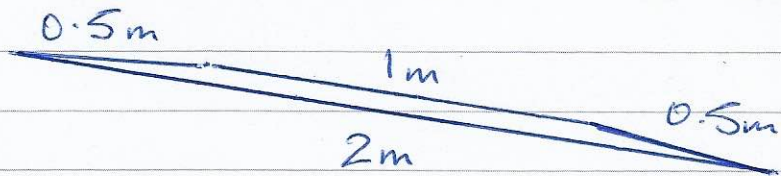
$$\theta = \frac{\pi}{180} \times :$$



$$\frac{p - p_{\infty}}{\frac{1}{2} \rho_{\infty} U_{\infty}^2} = \frac{\pi}{180} \times \frac{2}{\sqrt{M_{\infty}^2 - 1}} \times :$$



Surface lengths :
($\cos 4^\circ \approx 1$) :



(i) Add resolved force contributions for drag:

$$D = \frac{1}{2} \rho_{\infty} U_{\infty}^2 \cdot \frac{\pi}{180} \cdot \frac{2}{\sqrt{M_{\infty}^2 - 1}} \left[0.5 \cdot (-2) \cdot (-\sin 2^\circ) + 1 \cdot (-6) \cdot (-\sin 6^\circ) + 0.5 \cdot (-10) \cdot (-\sin 10^\circ) + 2 \cdot (+6) \cdot \sin 6^\circ \right]$$

0.01781 2.785

$$C_D = \frac{D}{\frac{1}{2} \rho_{\infty} U_{\infty}^2 \cdot 2 \text{ chord}} = 0.0248$$

N.B. $\sin \theta \approx \theta$
also OK

b)(ii) Work with forces $\perp$ chord, again with $\cos 4^\circ \approx 1$
(though here any error cancels with same approx for lengths!)

$$\uparrow F = \frac{1}{2} \rho_w U_\infty^2 \times \frac{\pi}{180} \times \frac{2}{\sqrt{M_\infty^2 - 1}} \times : \quad \begin{array}{ccc} 1 & 6 & 5 \\ & 12 & \end{array}$$

$$M = \frac{1}{2} \rho_w U_\infty^2 \times \frac{\pi}{180} \times \frac{2}{\sqrt{M_\infty^2 - 1}} \times \left[\underset{\substack{\uparrow \\ \text{moment arm}}}{0.25} \cdot 1 + 1.6 + 1.75 \cdot \underset{\substack{\uparrow \\ \text{force}}}{5} + 1.12 \right]$$

$$C_M = \frac{M}{\frac{1}{2} \rho_w U_\infty^2 c^2} = \underline{\underline{0.120}}$$

c) Linearised theory admits superposition,
i.e. we can calculate ΔC_M from change in geometry:

$$\Delta \theta = \frac{\pi}{180} \times : \quad \begin{array}{ccc} & & -8 \\ & & +8 \end{array}$$

$$\Delta \left(\frac{p - p_w}{\frac{1}{2} \rho_w U_\infty^2} \right) = \frac{\pi}{180} \times \frac{2}{\sqrt{M_\infty^2 - 1}} \times : \quad \begin{array}{ccc} & & -8 \\ & & +8 \end{array}$$

$$\Delta M = \frac{1}{2} \rho_w U_\infty^2 \times \frac{\pi}{180} \times \frac{2}{\sqrt{M_\infty^2 - 1}} \times 1.75 (8+8) \cdot 0.5$$

$$\Rightarrow \Delta C_M = \underline{\underline{0.062}}$$

- d) Implications:
- significant change in pitching moment affects balance, and hence tail design;
 - significant increase in drag expected from additional pressure forces, hence need more thrust to avoid performance degradation.

a) Check initial condition: $u(n,0) = \cos[k(n-0)] = \cos kn \checkmark$

Check equation: $\frac{\partial u}{\partial t} = ka \sin[k(n-a)]$

$$\frac{\partial u}{\partial n} = -k \sin[k(n-a)]$$

So $\frac{\partial u}{\partial t} + a \frac{\partial u}{\partial n} = 0$, and the equation is satisfied.

b)(i) Substitute the claimed solution into truncated equivalent PDE:

$$\underbrace{\frac{dA}{dt} \cos[k(n-at)]}_{\partial u / \partial t} + \underbrace{ka A \sin[k(n-at)] + a \{-kA \sin[k(n-at)]\}}_{\partial u / \partial n} = \underbrace{-v_{\text{eff}} k^2 A \cos[\dots]}_{-\partial^2 u / \partial n^2}$$

$\sin[\dots]$ terms cancel, and remaining equation is required to be true for all n, t ...

$$\frac{dA}{dt} = -v_{\text{eff}} k^2 A \Rightarrow A = A_0 e^{-v_{\text{eff}} k^2 t}$$

Initial condition $A(0) = 1 \Rightarrow A = \underline{\underline{e^{-v_{\text{eff}} k^2 t}}}$

(ii) For the scheme to be stable, v_{eff} must be +ve (otherwise we see exponential growth). Hence we require $\alpha \leq 1$ or, equivalently, $a \Delta t \leq \Delta n$.

When stable with $v_{\text{eff}} > 0$, A decays from its initial value of 1, when it should stay constant. This inaccuracy is mitigated by keeping α near 1 (if possible) and/or minimising Δn .

c) (i) First derive the new equivalent PDE:

$$u_i^{n+1} - u_i^{n-1} = \frac{-a \Delta t}{\Delta x} (u_{i+1}^n - u_{i-1}^n) \Rightarrow \frac{u_i^{n+1} - u_i^{n-1}}{\Delta t} = -a \frac{u_{i+1}^n - u_{i-1}^n}{\Delta x}$$

$$\text{Now } u_i^{n+1} = u_i^n + \frac{\partial u}{\partial t} \Delta t + \frac{\partial^2 u}{\partial t^2} \frac{\Delta t^2}{2} + \frac{\partial^3 u}{\partial t^3} \frac{\Delta t^3}{6} + \frac{\partial^4 u}{\partial t^4} \frac{\Delta t^4}{24} + O(\Delta t^5)$$

$$\text{and } u_i^{n-1} = u_i^n - \dots + \dots - \dots + \dots + O(\Delta t^5)$$

$$\text{So } \frac{u_i^{n+1} - u_i^{n-1}}{\Delta t} = 2 \left(\frac{\partial u}{\partial t} + \frac{\partial^3 u}{\partial t^3} \frac{\Delta t^2}{6} + O(\Delta t^4) \right)$$

Applying the same approach to the term $(u_{i+1}^n - u_{i-1}^n)/\Delta x$:

$$2 \left(\frac{\partial u}{\partial x} + \frac{\partial^3 u}{\partial x^3} \frac{\Delta x^2}{6} + O(\Delta x^4) \right) = -2a \left(\frac{\partial u}{\partial x} + \frac{\partial^3 u}{\partial x^3} \frac{\Delta x^2}{6} + O(\Delta x^4) \right)$$

leading to the following truncated equivalent PDE:

$$\frac{\partial u}{\partial t} + a \frac{\partial u}{\partial x} = - \frac{\Delta t^2}{6} \frac{\partial^3 u}{\partial t^3} - \frac{a \Delta x^2}{6} \frac{\partial^3 u}{\partial x^3}$$

For the claimed solution

$$\frac{\partial u}{\partial t} = kc \sin[k(x-ct)] \quad \frac{\partial^3 u}{\partial t^3} = -(kc)^3 \sin[k(x-ct)]$$

$$\frac{\partial u}{\partial x} = -k \sin[k(x-ct)] \quad \frac{\partial^3 u}{\partial x^3} = k^3 \sin[k(x-ct)]$$

Substitute into equivalent PDE ...

$$k(c-a) = (kc)^3 \frac{\Delta t^2}{6} - a k^3 \frac{\Delta x^2}{6}$$

This confirms $c \approx a$, so $c^3 = a^3 + \text{higher order}$

$$\text{and } k(c-a) = \frac{k^3}{6} \left[a^3 \Delta t^2 - a \Delta x^2 \right] \text{ to leading order}$$

$$c-a = \frac{k^2 a (a^2 - 1) \Delta x^2}{6}$$

Alternatively, note that $\frac{\partial u}{\partial t} = -a \frac{\partial u}{\partial x} + \text{higher order}$

$$\text{so } \frac{\partial^3 u}{\partial t^3} = -a^3 \frac{\partial^3 u}{\partial x^3} + \text{higher order},$$

and substitute for $\partial^3 u / \partial t^3$ before inserting claimed sol'n.

- (ii) The solution to the equivalent problem travels at speed c rather than $a \Rightarrow$ false convection.

Furthermore, the factor k^2 in $c-a$ shows that the speed error depends on wavelength $\Rightarrow$ dispersion.

$$a) (i) \quad \frac{dp_0}{dr} = 0, \quad \frac{dV_n}{dr} = \frac{1}{\sqrt{2}} \frac{dV}{dr}, \quad \frac{dV_\theta}{dr} = \frac{1}{\sqrt{2}} \frac{dV}{dr}$$

$$\text{so} \quad 0 = \frac{1}{2} V \frac{dV}{dr} + \frac{V}{2r} \left(V + r \frac{dV}{dr} \right)$$

$$V \frac{dV}{dr} + \frac{V^2}{2r} = 0$$

$$\frac{dV}{V} = -\frac{1}{2} \frac{dr}{r}$$

$$\text{Integrate} \quad \ln V = \text{const} - \frac{1}{2} \ln r, \quad \text{or} \quad V = c/r^{1/2}$$

$$V = V_H @ r = r_H \Rightarrow V = V_H \left(\frac{r_H}{r} \right)^{1/2}$$

$$=$$

$$(ii) \quad \dot{m} = \int_{r_H}^{r_T} \rho V_n dA \quad \text{with } dA = 2\pi r dr$$

$\uparrow$ N.B. Axial component

$$= \frac{2\pi\rho}{\sqrt{2}} V_H r_H^{1/2} \int_{r_H}^{r_T} r^{1/2} dr$$

$$= \frac{2\sqrt{2}\pi}{3} \rho V_H r_H^{1/2} \left[r_T^{3/2} - r_H^{3/2} \right]$$

$$=$$

$$b) \quad \delta u = \frac{\partial u}{\partial t} \delta t + \frac{\partial u}{\partial x} \delta x$$

$$\text{Along } x = X(t), \quad \delta x = \dot{X}(t) \delta t \Rightarrow \delta u = \left(\frac{\partial u}{\partial t} + \frac{\partial u}{\partial x} \dot{X} \right) \delta t$$

$$=$$

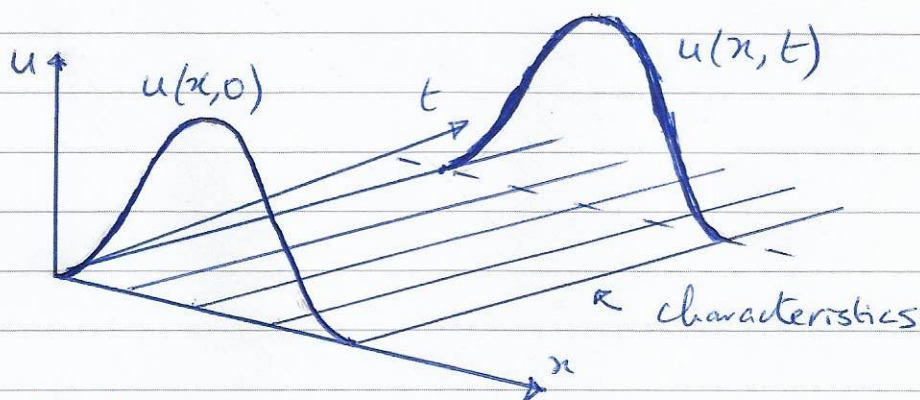
c) Along a characteristic, $\delta u = 0$

i.e., from (b), $\frac{\partial u}{\partial t} + \dot{X} \frac{\partial u}{\partial x} = 0$, where $x = X(t)$ is the equation of the characteristic

$\therefore$ By comparison with the general form of the convection eqn,

$$\dot{X} = f(u)$$

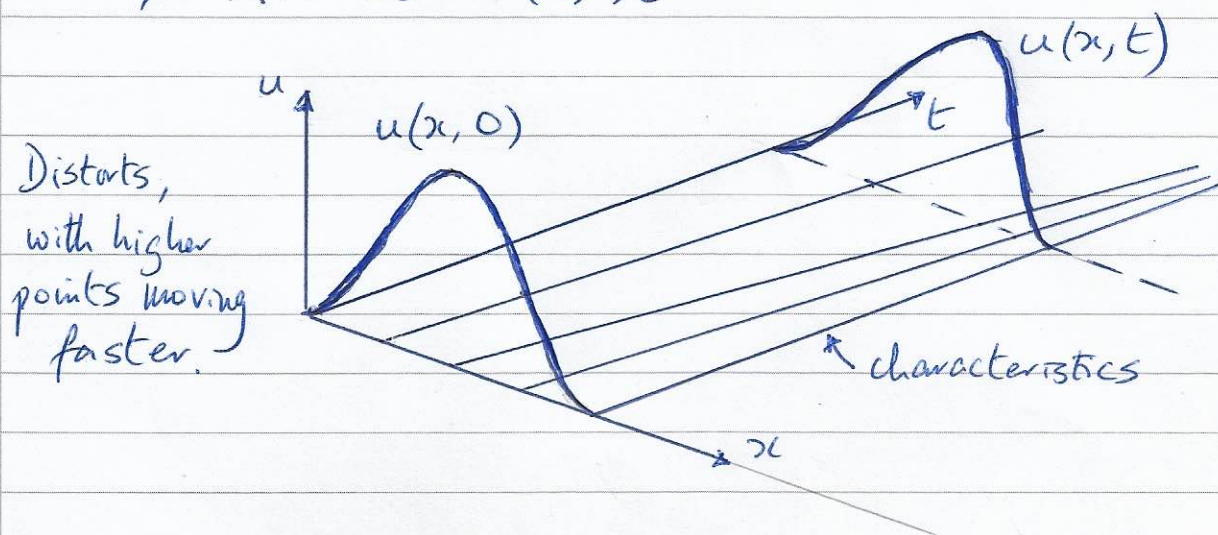
(i) $f(u) = a \Rightarrow X = x_0 + at$



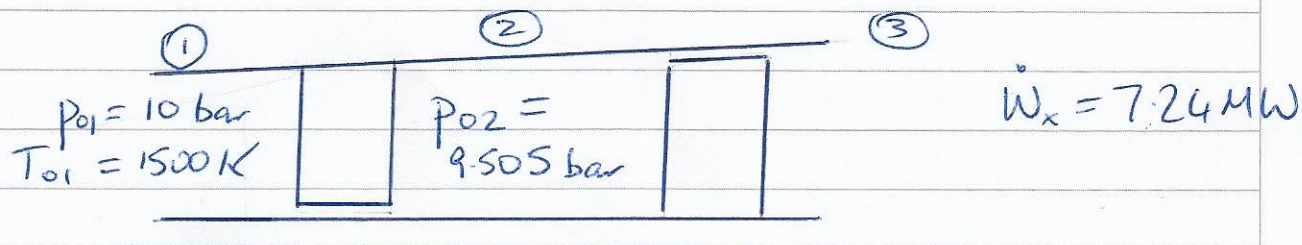
Convects downstream
at speed a ; no change in shape.

(ii) $f(u) = u$, and by definition $u = \text{const}$ on a char

$$\Rightarrow X = x_0 + u(x_0, 0)t$$



Distorts,
with higher
points moving
faster.



a) (i) Conditions at (2): $T_{02} = T_{01}$ (adiabatic, no work)

$$0.1(P_{02} - P_2) = P_{01} - P_{02} \Rightarrow P_2 = 4.555$$

$$P_2 / P_{02} = 0.4792 \Rightarrow M_2 = 1.1007$$

$$\text{so } T_2 = T_{02} \left(1 + \frac{\gamma-1}{2} M_2^2\right)^{-1} = 1248.2 \text{ K}; a_2 = \sqrt{\gamma R T_2} = 691.0 \text{ m/s}$$

Don't forget $\gamma = 1.333$ here!

$$\text{Thus } V_2 = a_2 M_2 = 760.6 \text{ m/s}$$

$$\rho_2 = P_2 / RT_2 = 1.2715 \text{ kg/m}^3$$

$$\dot{m} = \rho_2 A_2 V_2 \cos \alpha_2 = \underline{\underline{37.4(1) \text{ kg/s}}}$$

$$\pi(r_1^2 - r_2^2) = 0.11310 \rightarrow$$

(ii) Quantities from calc: stagnation-pressure loss, flow angle

P_0 loss: depends on non-ideal effects, so difficult to calculate accurately; $0.1 \rightarrow 0.11$ gives $P_{02} = 5.005 \text{ bar}$
 $0.1 \rightarrow 0.09$ gives $P_2 = 4.005 \text{ bar}$

α_2 : calculation likely less tricky, but even 1° error changes $\cos \alpha_2$ by 5% (v.i.e. direct calc)

$\Rightarrow$ errors in region of 10% could easily arise from either of the quantities estimated numerically.

$$b)(i) \quad \eta_{TS} = \frac{\text{actual work}}{\text{ideal work}} = \frac{h_{01} - h_{03}}{h_{01} - h_{03i}}$$

$$h_{01} - h_{03} = \dot{W}_x / \dot{m} = 193.5 \times 10^3 \text{ J/kg}$$

$$h_{03i} = c_p T_{03i} = c_p T_{01} \left(\frac{p_{03}}{p_{01}} \right)^{\frac{\gamma-1}{\gamma}} = c_p \cdot 134.9$$

$$\text{so } h_{01} - h_{03i} = 212.7 \times 10^3 \text{ J/kg, and } \eta_{TS} = \underline{\underline{0.910}}$$

(ii) Not possible to consider detail control-volume analysis (1st or 2nd law) without additional information. However, we do know that the cooling air mixes with the main flow, and that this will involve irreversible heat and momentum transfer. These phenomena will tend to decrease the efficiency.

c) Rotational speed measurement would yield blade speed, and hence allow us to apply the Euler work eqn:

$$\dot{W}_x = U \Delta V_\theta \quad \text{over rotor.}$$

In conjunction with continuity ($\dot{m} = \rho_3 A_3 V_{x3}$), this allows conditions at rotor exit to be determined. (In practice, some iteration required.)

Other viable answers, given suitable justification:

flow coefficient; stage-loading coefficient; α_{2r} ; blade forces